

# Hydrodynamics Study of a Bubbling Fluidized Bed

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## Abstract

**Hydrodynamic behavior of a bubbling fluidized bed was computationally analyzed in a 2D model. Different drag models were used to understand the variations of particle velocity and volume fraction at a certain bed height.**

**Keywords: Bubbling fluidized bed, Volume fraction, Drag models**

## Nomenclature

2D	2-Dimensional
K	Momentum exchange coefficient
d	Diameter
$C_D$	Drag Coefficient
V	Velocity
g	Gas
s	Solid
p	Particle
$V_{r,s}$	Terminal velocity for solid phase

### Greek Symbols

$\alpha$	Volume fraction
$\rho$	Density
$\mu$	Dynamic viscosity
$\tau$	Particulate relaxation time

### Non-dimensional Numbers

Re	Reynolds number
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## 2. Numerical Description

**Table 1. Geometry and Computational Details**

Parameter	Detail
Model	2D
Dimensions	0.4 m $\times$ 0.155 m ( $\times$ 0.02 m)
Geometry and Mesh utility	blockMesh
Post-processing tool	Paraview, Sigma Plot
Solver	twoPhaseEulerFoam
Pressure-velocity coupling	PIMPLE algorithm [5]
Convective term solving scheme	V scheme [5]
Turbulent term solving scheme	Gauss limitedLinear [5]
Drag models	GidaspowErgunWenYu, Schiller–Naumann, Syamlal-O'Brien

## 1. Introduction

Fluidization is a process in which solid particles behaves as fluid due to suspension of a gas or liquid. This operation is generally used in industrial processes like catalytic reactions, particle coating, heating, cooling and drying etc. The physics behind the fluidization shows the significance of particle velocity, particle volume fraction, minimum fluidization velocity etc.

The velocity profile and volume fraction profile of particles have been analyzed and reported in this study.

**Table 2. Solid properties and initial conditions**

Parameter	Value/Condition
$\rho$	2500 kg/m <sup>3</sup>
$d_p$	350 microns
$\Phi$	0.6
e	0.99
$V_{air}$	0.587 m/sec
$V_{wall}$	Johnson-Jackson slip
Initial bed height	0.2 m
Initial solid $\alpha$	40 %

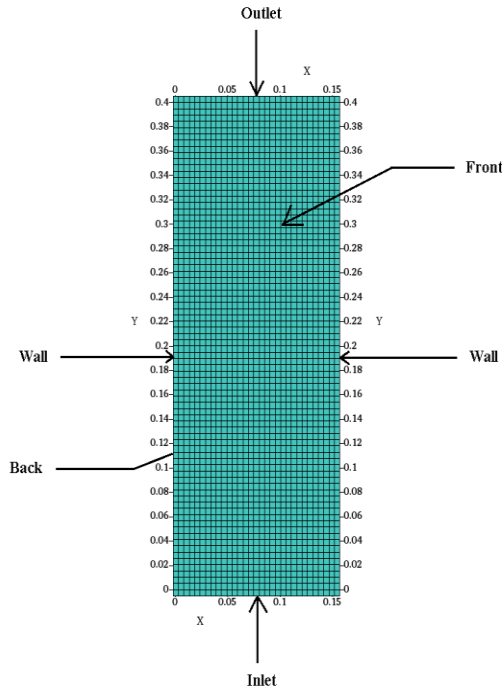


Fig. 1. 2D domain for numerical analysis

### 3. Drag Model Equations

#### 3.1. GidaspowWenYu model:

Wen-Yu model (1966)

$$K_{gs} = \frac{3}{4} C_D \frac{\alpha_g \alpha_s \rho_g}{d_p \alpha_g^{2.65}} \left| \vec{v}_g - \vec{v}_s \right|$$

Gidaspow model (1994)

$$K_{gs} = 150 C_D \frac{\alpha_s \mu_g}{\alpha_g d_p^2} (1 - \alpha_g) + 1.75 \frac{\alpha_g \rho_g}{d_p} \left| \vec{v}_g - \vec{v}_s \right| \quad ; \text{ for } \alpha_g \leq 0.8$$

Now, GidaspowWenYu model; when  $\alpha_g \geq 0.8$

$$C_D = \frac{24}{\alpha_g Re_s} (1 + (0.15 \alpha_g Re_s)^{0.687})$$

$$Re_s = \rho_g \frac{d_p}{\mu_g} \left| \vec{v}_g - \vec{v}_s \right|$$

#### 3.2. Schiller-Naumann model:

$$K_{gs} = \frac{\alpha_g \alpha_s \rho_g f}{\tau_s}$$

$$\tau_s = \frac{\rho_s d_p^2}{18 \mu_g}$$

Where,  $f = \frac{C_D Re_s}{24}$  and,

$$C_D = \frac{24}{Re_s} (1 + (0.15 \alpha_g Re)^{0.687}) \quad ; \text{ for } Re \leq 1000$$

$$C_D = 0.44 \quad ; \text{ for } Re \geq 1000$$

$$Re_{gs} = \rho_g \frac{d_p}{\mu_g} \left| \vec{v}_g - \vec{v}_s \right|$$

#### 3.3. Syamlal-O'Brien model:

[2]

$$K_{gs} = \frac{3}{4} C_D \frac{\alpha_g \alpha_s \rho_g}{d_p} \left( \frac{Re_s}{v_{r,s}^2} \right) \left| \vec{v}_g - \vec{v}_s \right|$$

$$v_{r,s} = 0.5(A - 0.06 Re_s + \sqrt{((0.06 Re_s)^2 + 0.12 Re_s(2B - A) + A^2)})$$

Where,  $A = \alpha_g^{4.14}$  and

$$B = 0.8 \alpha_g^{1.28} \quad \text{for } \alpha_g \leq 0.85$$

$$B = 0.8 \alpha_g^{2.65} \quad \text{for } \alpha_g > 0.85$$

## 4. Results

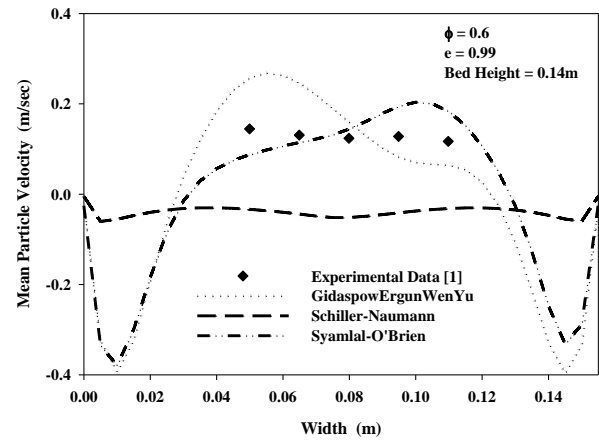


Fig. 2. Time-averaged particle velocity profiles at bed height = 0.14m

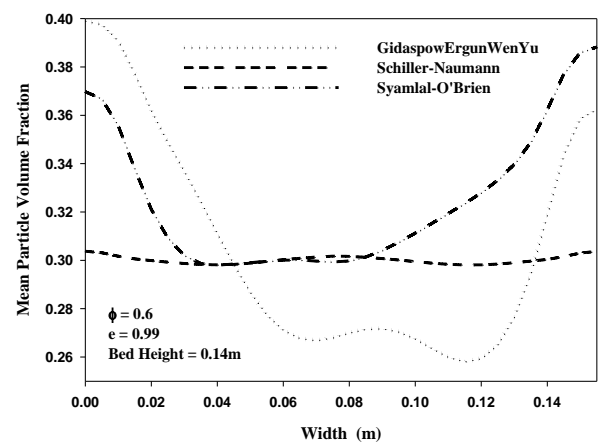
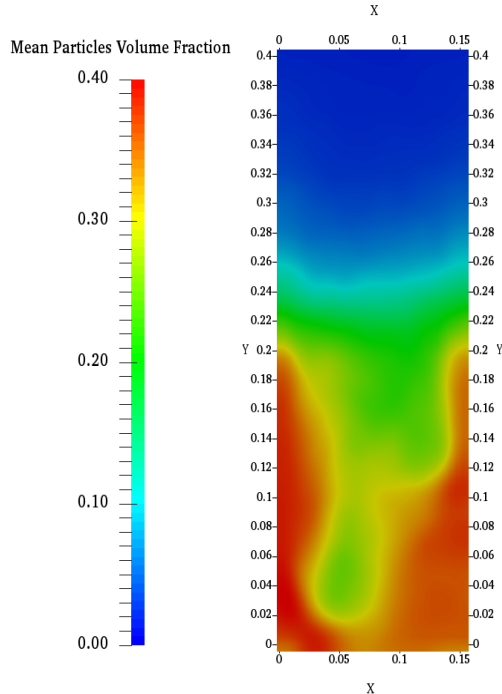


Fig. 3. Distributions of time-averaged particle volume fraction at bed height = 0.14m

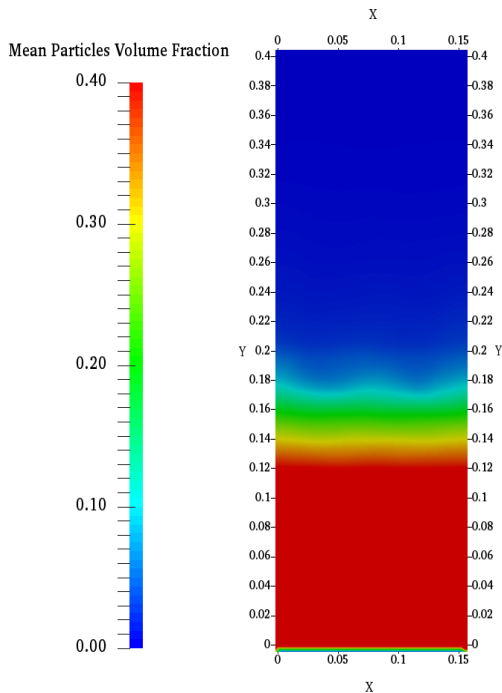
Fig. 2. explains that GidaspowErgunWenYu and Syamlal O'Brien provide almost closed particle velocity to the experimental velocity. But Schiller-Naumann results underpredicted particle velocity.

Again, Fig. 3. shows that volume fraction profiles are not so symmetric for the three drag models mentioned above.

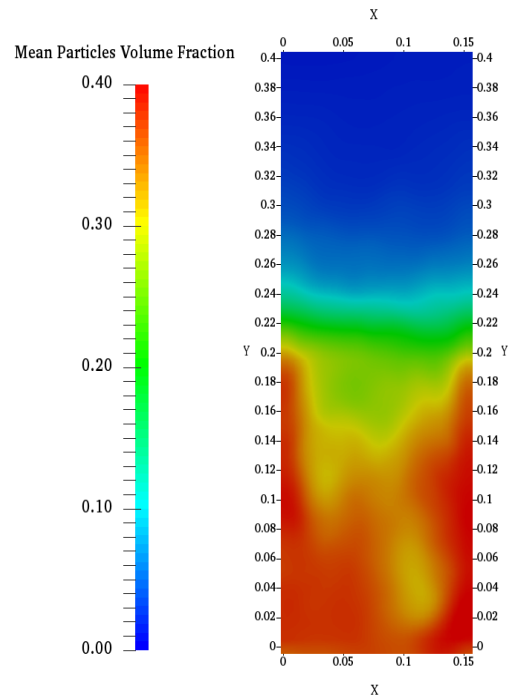
## 5. Contours



**Fig. 4. Time-averaged particle volume fraction for GidaspowErgunWenYu**



**Fig. 5. Time-averaged particle volume fraction for Schiller-Naumann**



**Fig. 6. Time-averaged particle volume fraction for Syamlal-O'Brien**

## References

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